

#### **PRODUCT SHEET**

# **CL Resin**

## **Main Applications**

- Separation of chloride and iodide

## **Packing**

Order N°.	Form	Particle size
CL-B25-A, CL-B50-A, CL-B100-A, CL-B200-A	25g, 50g, 100g and 200g bottles CL Resin	100-150 μm
CL-C20-A, CL-C50-A	Boxes of 20, 50 and 200 CL Resin columns	100-150 μm
CL-B25-S, CL-B50-S, CL-B100-S, CL-B200-S	25g, 50g, 100g and 200g bottles CL Resin	50-100 μm
CL-R10-S	10 2mL cartridges	50-100 μm
CL-B25-L, CL-B50-L, CL-B100-L, CL-B200-L	25g, 50g, 100g and 200g bottles CL Resin	150-300 µm

## Physical and chemical properties

Density: 0,37 g/ml

Capacity: 6,5 mg Cl<sup>-</sup>/g CL Resin (loaded with 20 mg Ag<sup>+</sup>)

25 mg I<sup>-</sup>/g CL Resin (loaded with 20 mg Ag<sup>+</sup>)

### **Conditions of utilization**

Recommended T of utilization: /

Flow rate : A grade: 0.6 – 0.8 mL/min Storage : Dry and dark, T<30°C

### **Methods**

Reference	Description	Matrix	Analytes	Support
TKI-CL01	CI-36 / I-129 separation	Environmental and decommissioning samples	Cl-36, I-129	Bulk, columns



#### **CL RESIN**

The CL Resin is used for the separation of chloride and iodide and is based on an extraction system that is selective for platinum group metals, gold and silver. The selectivity for halides is introduced by loading the resin with silver.

Table1 shows Dw values of selected cations on the CL Resin, for practical reasons sulphuric acid was chosen as extraction medium. It can be seen that the CL Resin has high selectivity for Pd and Ag, whereas the D<sub>W</sub> values of the other elements tested are low. Ag further shows high Dw values over a wide pH range (from 1M H<sub>2</sub>SO<sub>4</sub> to dilute sulphuric acid (pH 5)). It will thus be extracted or remain fixed over a wide range of pH values.

Table 1: Dw values CL Resin of selected cations in

sulphuric acid (data taken from (1)).							
Analyte	Extraction condition	D <sub>w</sub> , mL.g <sup>-1</sup>					
Ag	1M H <sub>2</sub> SO <sub>4</sub>	650000					
Ag	Sulfuric acid, pH 3	600000					
Ag	Sulfuric acid, pH 5	350000					
Cd	1M H <sub>2</sub> SO <sub>4</sub>	<1					
Ce	1M H <sub>2</sub> SO <sub>4</sub>	4					
Со	1M H <sub>2</sub> SO <sub>4</sub>	<1					
Cu	1M H <sub>2</sub> SO <sub>4</sub>	<1					
Fe	1M H <sub>2</sub> SO <sub>4</sub>	<1					
Mn	1M H <sub>2</sub> SO <sub>4</sub>	<1					
Ni	1M H <sub>2</sub> SO <sub>4</sub>	<1					
Pd	1M H <sub>2</sub> SO <sub>4</sub>	87000					
Zn	1M H <sub>2</sub> SO <sub>4</sub>	25					

The loading of the resin with silver cations allows good selectivity for anions, especially formina sparely or insoluble complexes. Dw values for chloride and iodide on the silver loaded CL Resin in 1M H<sub>2</sub>SO<sub>4</sub> were determined to be 1600 and 1980 respectively. Both are thus well retained under those conditions. The CL Resin used for the Dw experiments was loaded with 20 mg Ag+ per g of CL Resin prior to the extraction experiments

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which corresponds to a typical working capacity. The capacities for chloride and iodide of the silver loaded resin under these conditions are: 16.3 +/-1.6 mg iodide per 2 mL column (approx. 25 mg iodide per g resin) and 4.3 +/- 0.2 mg chloride per 2 mL column (approx. 6.5 mg chloride per g resin). Higher capacities for halides can be obtained by increasing the silver load of the CL

In order to evaluate best suited conditions for the separation of chloride and iodide Dw values of chloride and iodide were determined on silver loaded CL Resin in varying SCN- and S2concentrations: Fig. 1 and 2 show the obtained results.

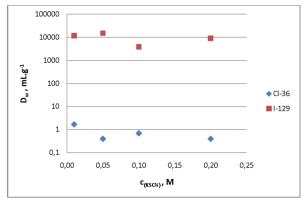


Figure 1: Dw of Cl and I on Ag+ loaded CL Resin at pH 7 and varying SCN<sup>-</sup> concentrations (1).

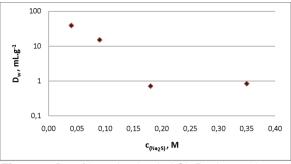


Figure 2: Dw of I on Ag+ loaded CL Resin at pH 7 and varying Na<sub>2</sub>S concentrations (1).

Chloride can be easily eluted from the resin using SCN solutions whereas iodide remains fixed. lodide can then be eluted from the resin using a high concentration solution of S2-. Based on this information, a method for the separation of chloride and iodide was developed and optimized by Zulauf et al. [1]; fig. 3 schematically shows this method. In order to assure that both chlorine and iodine are present as chloride and iodide, the sample might be loaded from a sulphuric acid solution containing 0.1M SnSO<sub>4</sub> as reducing agent. This is especially important in case of chlorine since e.g. chlorate is not fixed on the



resin, whereas iodate is extracted, as could be expected from silver salt solubility data.

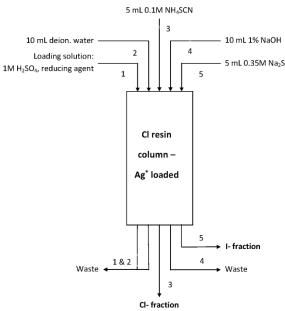


Figure 3: Scheme of optimized CI- / I- separation method (1).

The sample is preferably loaded onto the silver loaded CL Resin from 1M H<sub>2</sub>SO<sub>4</sub> (slightly acidic or even neutral conditions are also acceptable). During a first rinse (deionised water) matrix elements and potential interferents are removed from the column. Chloride is then eluted in a small volume of NH<sub>4</sub>SCN or NaSCN.

During method optimization it was shown that rinsing the column with a dilute alkaline solution before iodide elution lead to a strong increase of the iodide yield. Therefore, the CL Resin column is accordingly rinsed with 1% NaOH before iodide is finally eluted in a small volume of a Na<sub>2</sub>S solution (Remark: all work with the Na<sub>2</sub>S solutions should be performed under a fume hood, including the addition of the liquid scintillation cocktail.).

The small elution volumes used for elution allow for direct measurement of the obtained fractions by LSC (Remark: some LSC cocktails reduce traces of Ag+ co-eluted from the column resulting in 'blackened' LSC samples; it is thus advisable to test your cocktail before use. ProSafe HC was found to be a suitable cocktail).

Fig. 4 shows the result of an elution study performed using a solution containing Cl-36 and I-129 as chloride and iodide respectively. Both Cl-36 and I-129 are quantitatively recovered in a small volume of the respective eluting agent, the separation of both is very clean.

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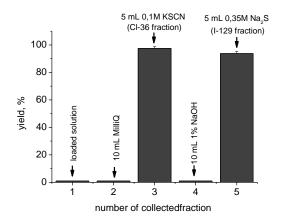


Figure 4: Elution profile of combined <sup>36</sup>Cl and <sup>129</sup>I with optimized method, 2 mL CL Resin column (Ag<sup>+</sup> loaded).

In order to obtain additional information on the purity of the chloride and iodide fractions decontamination factors (D<sub>f</sub>) were determined by applying the optimized method to several multielement solutions and solutions of radioactive standards, table 2 summarizes the results.

**Table 2:** Decontamination factors Df of various elements in chloride and iodide fractions.

elements in c	elements in chloride and lodide fractions.							
Analyte	D <sub>f</sub> in Cl <sup>-</sup> fraction	D <sub>f</sub> in I <sup>-</sup> fraction						
Ba	>1000	>600						
Cd	>6900	>7700						
Co	>170	>1500						
Cs	>200	>6200						
Cu	>210	>190						
Mn	>210	>370						
Ni	>170	>320						
Pb	>300	>720						
Sr	>180	>17000						
U	>1900	>200						
<sup>60</sup> Co	>320	>320						
<sup>137</sup> Cs	>150	>150						
<sup>90</sup> Sr/ <sup>90</sup> Y	>180	>160						
<sup>36</sup> CI	NA	>160						
129	>420	NA						

Overall the method shows very good selectivity for chloride and iodide.

Mean chemical yields of the separation were found to be 97.0 %  $\pm$  2.5% (k=1, N=30) for chloride and 91.7% %  $\pm$  10.1% (k=1, N=30) for iodide [1]. These yields were then applied to the analysis of spiked tap water samples (defined Cl-36 and I-129 activities plus approx. 17 Bq each of Co-60, Sr-90 and Cs-137). Table 3 compares obtained and spiked activities, both agree very



well. Even though results obtained applying fixed separation yields were found to be very satisfying it is advisable to perform a yield determination (e.g. *via* ion chromatography) if possible.

**Table 3:** Comparison determined vs. added activities, spiked tap water samples, 3 replicates, bias and  $E_n$ , k=2.

	determine	d activities	added a	added activities		
I-129	A(I-129)	U <sub>A(I-129)</sub>	A(I-129)	U <sub>A(I-129)</sub>	Bias	_
1-129	/ Bq	/ Bq	/ Bq	/ Bq	/%	E <sub>n</sub>
Repl. 1	8,24	1,98	8,22	1,31	0,3%	0,01
Repl. 2	8,17	1,97	8,22	1,31	-0,5%	0,02
Repl. 3	7,86	1,89	8,22	1,31	-4,4%	0,16
Cl-36	A(Cl-36)	U <sub>A(CI-36)</sub>	A(Cl-36)	U <sub>A(CI-36)</sub>	Bias	E <sub>n</sub>
CI-30	/ Bq	/ Bq	/ Bq	/ Bq	/%	
Repl. 1	8,97	1,05	9,44	0,94	-5,1%	0,34
Repl. 2	9,11	1,06	9,44	0,94	-3,5%	0,23
Repl. 3	9,12	1,06	9,44	0,94	-3,5%	0,23

A similar experiment was performed at the SUBATECH laboratory in France [2]. Four effluent samples were spiked (Samples Cl1 and Cl2 with identical amounts of Cl-36 and no I-129; sample Cl3 with Cl-36 and I-129 at an activity ratio of 1:1 and sample Cl4 with Cl-36 and I-129 at an activity ratio of 1:10) and analysed for Cl-36 activity. Table 4 summarizes the obtained results [2]. Obtained and reference activities agree very well. Even at high I-129 excess no positive bias is introduced into the Cl-36 results, further stating the clean chloride/iodide separation. The standard deviation of the results obtained for samples Cl1 and Cl2 is 3.7% (N = 2, k = 1) thus confirming the good repeatability of the separation.

**Table 4:** Comparison determined vs. reference activities, spiked effluent samples, bias and zeta values.

		-36 cal activity	I-1 Theoretic			Perkin Elmer TriCarb 3190TR/SL			Comparison of CI-36 activity	
Sample	A (Bq.L <sup>-1</sup> )	U <sub>A</sub> (Bq.L <sup>-1</sup> )	A (Bq.L <sup>-1</sup> )	U <sub>A</sub> (Bq.L <sup>-1</sup> )	tSIE	cpm	A (Bq.L <sup>-1</sup> )	U <sub>A</sub> (Bq.L <sup>-1</sup> )	Deviation (%)	Zeta test
CI0	Blank	-	Blank	-	236.3	5.22	<lod< td=""><td>-</td><td>-</td><td>-</td></lod<>	-	-	-
CI1	1.873E+04	6.556E+02	0	-	239.8	1774.8	1.809E+04	1.191E+03	-3.44	0.47
CI2	1.873E+04	6.556E+02	0	-	243.9	1871.4	1.905E+04	1.255E+03	1.72	0.23
CI3	1.873E+04	6.556E+02	1.889E+04	5.100E+02	252.0	1865.3	1.806E+04	1.189E+03	-3.57	0.49
C14	1.873E+03	6.556E+01	1.897E+04	5.121E+02	254.2	189.85	1.792E+03	1.226E+02	-4.35	0.59

In addition to aqueous samples Zulauf et al. [3] also tested the separation method on spiked soil, concrete and membrane filter samples.

In a first step mean chloride and iodide leaching yields were determined for the three matrices. Samples (approx. 250 mg) of each material were spiked with Cl-36, I-129 respectively, dried and then leached with 1M NaOH for 4h at 70°. The Cl-36 or I-129 activity of the leaching solutions was then determined via

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liquid scintillation counting. Leaching yields obtained were generally > 90%.

Fresh sets of spiked samples were then prepared by spiking the respective matrix with defined amounts of Cl-36 and I-129, followed by a drying step. The dried samples were then leached and separated as described before. Analyses were performed in triplicate, mean leaching and separation yields were assumed for activity calculation. Tables 5a-c summarize the obtained results.

**Table 5a:** Comparison determined vs. reference activities, soil, 3 replicates, bias and  $E_n$ , k=2.

		determined	activities	reference	activities		
	<sup>129</sup>	A( <sup>129</sup> l) , Bq	U <sub>A(129I)</sub> , Bq	A( <sup>129</sup> I) , Bq	U <sub>A(129I)</sub> , Bq	Bias , %	En
	Repl. 1	7.65	1.59	8.22	1.31	-6.94	0.28
	Repl. 2	7.60	1.58	8.22	1.31	-7.49	0.30
_	Repl. 3	7.47	1.56	8.22	1.31	-9.09	0.37
lios	<sup>36</sup> CI	A( <sup>36</sup> CI) , Bq	U <sub>A(36CI)</sub> , Bq	A( <sup>36</sup> Cl) , Bq	U <sub>A(36CI)</sub> , Bq	Bias , %	En
	Repl. 1	9.39	1.76	9.44	0.94	-0.55	0.03
	Repl. 2	9.59	1.79	9.44	0.94	1.60	0.07
	Repl. 3	9.55	1.79	9.44	0.94	1.20	0.06

**Table 5b:** Comparison determined vs. reference activities, concrete, 3 replicates, bias and  $E_n$ , k=2.

		determine	dactivities	reference activities			
	<sup>129</sup> l	A( <sup>129</sup> I) , Bq	U <sub>A(1291)</sub> , Bq	A( <sup>129</sup> I) , Bq	U <sub>A(129I)</sub> , Bq	Bias , %	En
	Repl. 1	7.71	1.96	8.22	1.31	-6.22	0.22
	Repl. 2	7.74	1.97	8.22	1.31	-5.83	0.20
ete	Repl. 3	7.61	1.94	8.22	1.31	-7.36	0.26
concrete	<sup>36</sup> CI	A( <sup>36</sup> CI) , Bq	U <sub>A(36CI)</sub> , Bq	A( <sup>36</sup> Cl) , Bq	U <sub>A(36CI)</sub> , Bq	Bias , %	En
	Repl. 1	9.40	1.56	9.44	0.94	-0.47	0.02
	Repl. 2	9.32	1.54	9.44	0.94	-1.30	0.07
	Repl. 3	9.35	1.55	9.44	0.94	-0.91	0.05

**Table 5c:** Comparison determined vs. reference activities, filter, 3 replicates, bias and  $E_n$ , k=2.

		determined	activities	reference	activities		
	<sup>129</sup> [	A( <sup>129</sup> I) , Bq	U <sub>A(129I)</sub> , Bq	A( <sup>129</sup> I) , Bq	U <sub>A(129I)</sub> , Bq	Bias , %	E <sub>n</sub>
	Repl. 1	7.89	2.82	8.22	1.31	-4.04	0.11
	Repl. 2	8.28	2.96	8.22	1.31	0.78	0.02
ē	Repl. 3	7.58	2.71	8.22	1.31	-7.79	0.21
filter	<sup>36</sup> CI	A( <sup>36</sup> CI) , Bq	U <sub>A(36CI)</sub> , Bq	A( <sup>36</sup> CI) , Bq	U <sub>A(36CI)</sub> , Bq	Bias , %	En
	Repl. 1	9.58	1.47	9.44	0.94	1.46	0.08
	Repl. 2	9.20	1.41	9.44	0.94	-2.52	0.14
	Repl. 3	9.70	1.48	9.44	0.94	2.71	0.15

Overall determined and reference activities agree very well, however especially for concrete and soil samples I-129 results show a slight



negative bias, determining the chemical yield of the separation is thus advisable and will lead to further improvement of the accuracy of the method.

Warwick et al. [4] developed a method for the analysis of decommissioning samples (e.g. spent resin) based on another sample preparation type. Their method is based on the thermal decomposition of the sample to be analysed using a 'Pyrolyser' furnace. Volatilized chlorine species are transported by a stream of moistened air into a bubbler containing a 6 mM Na<sub>2</sub>CO<sub>3</sub> solution where they are retained. Mean recovery of this sample treatment step was found to be 86%.

The bubbler solution is then directly loaded onto silver loaded CL Resin. The authors found that, since the sample is not loaded from a highly acidic sample solution, an additional rinsing step is necessary ('modified wash') in order to improve C-14 decontamination. Fig. 5 shows the developed and optimized method.

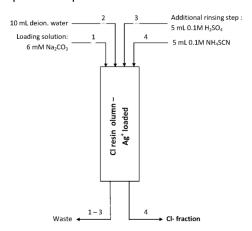


Figure 5: Scheme of Ct / l' separation method optimized for use with RADDEC's Pyrolyser (4).

Table 6 shows the decontamination factors for the CI fraction obtained by the authors ("modified wash" is referring to results obtained using the method including the additional rinse with dilute sulphuric acid). Decontamination factors obtained are high; the additional wash significantly improved C-14 decontamination of the CI fraction.

The overall yield of the method (pyrolyser step plus column separation) was found to be close to 86% which allowed obtaining a detection limit of 20 mBq.g<sup>-1</sup> for a sample mass of 1g, a liquid scintillation counting efficiency of 98% and 180 min counting time.

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**Table 6:** Decontamination factors of Pyrolyser / CL Resin based method [4].

	<sup>36</sup> CI fraction	129  fraction
3НТО	> 500	> 2000
<sup>14</sup> CO <sub>3</sub>	7	5000
<sup>14</sup> C modified wash	700	
35S modified wash	1500	1000
36 <b>CI</b>		> 2000
129	1300	

The method was further tested on a spent resin sample. A very good agreement between the specific activity determined through the pyrolyser / CL Resin method (4.3±0.1 kBq) and the expected value (4.1 kBq) was found [4].

#### **Bibliography**

- (1) A. Zulauf, S. Happel, M. B. Mokili, A. Bombard, H. Jungclas: Characterization of an extraction chrom atographic resin for the separation and determination of <sup>36</sup>Cl and <sup>129</sup>I. *J. Radanal Nucl Chem*, 286(2), 539-546 (DOI: 10.1007/s10967-010-0772-5)
- (2) A. Zulauf, S. Happel, M. B. Mokili, P. Warwick, A. Bombard, H. Jungclas: Determination of Cl-36 and I-129 by LSC after separation on an extraction chromatographic resin. Presentation at the LSC 2010 conference, 07/09/2010, Paris (France), available online: <a href="http://www.nucleide.org/LSC2010/presentations/0-56.pdf">http://www.nucleide.org/LSC2010/presentations/0-56.pdf</a>.
- (3) A. Zulauf, S. Happel: Characterisation of a CI- and I-selective resin. Presentation at the TrisKem International users group meeting, 14/09/2010, Chester (UK); available online: <a href="http://www.triskem-international.com/iso-album/ugm-chester-06-zulauf-hap-pel-cl-resin.pdf">http://www.triskem-international.com/iso-album/ugm-chester-06-zulauf-hap-pel-cl-resin.pdf</a>.
- (4) P E Warwick, A Zulauf, S Happel, I W Croudace: Determination of <sup>36</sup>Cl in decommissioning samples using a Pyrolyser furnace and extraction chromatographic separations. Presentation at the 11th ERA Symposium, 16/09/2010, Chester (UK); available online: <a href="http://www.triskem-international.com/iso-album/11">http://www.triskem-international.com/iso-album/11</a> era chester warwick det ermination of 36cl in decommissioning samples using a pyrolyser.pdf.